

# Uncertainty Quantification in Simulations of Reactive Flows Part 2: Applications

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## UQ in Reacting Flows

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### **Planetary Entry Simulations**

**High-Temperature Reactive Flow** 

 During descent in the atmosphere vehicles experience extreme heating loads



- The design of the thermal protection system (TPS) is the most critical component of every planetary entry mission
- TPS design is fundamentally computation-based because no ground-test can reproduce all the aspects of flight
- Safety (and reliability) requires rigorous evaluation of the uncertainties present

### Jupiter Entry Probe - Galieo



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Source: NASA

### **Titan Entry Simulations**

High-Temperature Reactive Flow

Predictions of TPS heating loads re-entry are challenging

- Physics Components
  - Chemistry
  - Radiation
  - Turbulence
  - etc.
- Computational issues
  - Strong shocks
  - Thin boundary layers
  - Flow separation
  - etc.

We focus on the uncertainties in the chemical kinetics, and their impact on the heat transfer at the stagnation point...

### **Titan Entry Simulations**

Aero-thermodynamic model

We consider *nominal* conditions for the Titan entry:

#### Table: Freestream conditions

N <sub>2</sub>	CH <sub>4</sub>	$ ho_{\infty}(kg/m^3)$	$V_{\infty}(km/s)$	$T_{\infty}(K)$
95%	5%	$1.49 \times 10^{-4}$	5.76	152.7



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### **Titan Entry Simulations**

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The strong bow shock induced strong non-equilibrium effects and dissociation/ionization

- We assumed a 13-species mechanism:
- ▶ C, H, N, C<sub>2</sub>, CH<sub>4</sub>, CH<sub>3</sub>, CH<sub>2</sub>, CH, CN, H<sub>2</sub>, HCN, N<sub>2</sub>, NH
- 26 reactions: 12 dissociation & 14 exchange

### Probabilistic approach

Reaction rates in ionization/dissociation models

- Uncertainty in the reactions rates, gathered from
  - theory
  - experiments
  - engineering judgment
- Uncertainty in the reaction rates is described using independent

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	Dissociation reactions $k = A_r T^{br} \exp(-C_r/T)$	Ar(cc/mol-s)	b <sub>r</sub>	C <sub>7</sub> (K)	95% conf. limit [Ref.]
1	$N_2 + M \Leftrightarrow 2N+M$	7.00×10 <sup>21</sup>	-1.60	113200	See Table 2
	M=N,C,H	3.00×10 <sup>22</sup>	-1.60	113200	
2	$CH_4 + M \Leftrightarrow CH_3 + H + M$	4.70×1047	-8.20	59200	±0.30[22]
3	$CH_1 + M \Leftrightarrow CH_2 + H + M$	1.02×10 <sup>16</sup>	0.00	45600	±0.35[22]
4	$CH_3 + M \Leftrightarrow CH + H_2 + M$	5.00×1015	0.00	42800	±0.30[23]
5	$CH_1 + M \Leftrightarrow CH + H + M$	4.00×10 <sup>15</sup>	0.00	41800	±0.30[23]
6	$CH_2 + M \Leftrightarrow C + H_2 + M$	1.30×1014	0.00	29700	±0.30[23]
7	$CH + M \Leftrightarrow C + H + M$	1.90×1014	0.00	33700	±0.30[23]
8	$C_2 + M \Leftrightarrow 2C + M$	1.50×10 <sup>16</sup>	0.00	71600	±0.30[24]
9	$H_2 + M \Leftrightarrow 2H + M$	2.23×1014	0.00	48350	±0.30[22,25]
10	$CN + M \Leftrightarrow C + N + M$	2.53×1014	0.00	71000	±0.30[26,27]
11	$NH + M \Leftrightarrow N + H + M$	1.80×10 <sup>14</sup>	0.00	37600	±0.30[28]
12	$HCN + M \Leftrightarrow CN + H + M$	3.57×10 <sup>26</sup>	-2.60	62845	±0.30[29]
	Exchange reactions				
13	$CH_3 + H \Leftrightarrow CH_2 + H_2$	6.03×10 <sup>13</sup>	0.00	7600	±1.00[25]
14	$CH_2 + N_2 \Leftrightarrow HCN + NH$	4.82×10 <sup>12</sup>	0.00	18000	±1.00[28]
15	$CH_2 + N \Leftrightarrow HCN + H$	5.00×10 <sup>13</sup>	0.00	0	±1.00[30]
16	$CH_2 + H \Leftrightarrow CH + H_2$	6.03×10 <sup>12</sup>	0.00	-900	±0.87[25,28]
17	$CH + N_2 \Leftrightarrow HCN + N$	4.40×10 <sup>12</sup>	0.00	11060	±0.35[30]
18	$CH + C \Leftrightarrow C_2 + H$	2.00×10 <sup>14</sup>	0.00	0	±1.00[23]
19	$C_2 + N_2 \Leftrightarrow 2CN$	1.50×10 <sup>13</sup>	0.00	21000	±0.30[31]
20	$CN + H_2 \Leftrightarrow HCN + H$	2.95×10 <sup>5</sup>	0.00	1130	±0.60[32]
21	$CN + C \Leftrightarrow C_2 + N$	5.00×10 <sup>13</sup>	0.00	13000	±0.54[18]
22	$N + H_2 \Leftrightarrow NH + H$	1.60×1014	0.00	12650	±0.30[33]
23	$C + N_2 \Leftrightarrow CN + N$	5.24×10 <sup>13</sup>	0.00	22600	±0.50[T]
24	$C + H_2 \Leftrightarrow CH + H$	4.00×1014	0.00	11700	±0.30[34]
25	$H + N_2 \Leftrightarrow NH + N$	3.00×10 <sup>12</sup>	0.50	71400	±0.50[T]
26	$CH_4 + H \Leftrightarrow CH_3 + H_2$	1.32×10 <sup>4</sup>	3.00	4045	±0.30[22,25]

### Another uncertainty source

Radiation modeling

NASA has identified the heating from shock layer radiation due to the CN radical formed in the  $N_2/CH_4$  atmosphere as a primary uncertainty

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- State-of-the art knowledge during the design of the Huygen's probe was the Boltzmann model
- This led to overprediction of the heating rates - conservative design
- Recent work has lead to collisional-radiative (CR) models



- We used Monte Carlo sampling (10,000 runs) to study the effect of the kinetics uncertainties
- We employed the CR model but compared to NASA earlier work (with Boltzmann model) in an attempt to characterize the epistemic uncertainty

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Stagnation point heat flux (W/cm<sup>2</sup>)



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Both the mean and the variance of the heat loads are affected by the radiation model

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- Both the mean and the variance of the heat loads are affected by the radiation model
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- Correlate and rank the uncertainty sources

Correlation: based on cross-plots of output (amount of *CN*) vs. input (uncertainty in the reaction rates)

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ANOVA ANalysis Of Variance: separate the variance in factors contributed by each input uncertainty



#### 8 major contributors to uncertainty

CR Model: Ghaffari, Iaccarino, Magin, 2009

Boltzmann model: Bose & Wright, 2004

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Determination of Ignition Delay Time is an important design consideration, for example in air-breathing hypersonic propulsion systems



In scramjet there are two competing mechanism causing sudden ignition of mixture:

 Mixing-induced accumulation of radicals starts chain reaction

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Shock-induced radical farming

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- Mixing-induced accumulation of radicals starts chain reaction
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  - Integrate evolution of reacting mixture in homogeneous isochoric (constant volume) reactor
  - Hydrogen chemistry (9 species, 25 elementary reactions)

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What is the uncertainty?

## Hydrogen Chemistry

**Reaction Rate Uncertainties** 

- Rate (and their uncertainties) are available in the literature
- Modified Arrhenius form
   k = AT<sup>n</sup> exp(-E/RT)
- The uncertainty factor UF is such that [k/UF : k × UF] provide probable bounds!
- Assume that the reaction rate are independent, lognormally distributed r.v.

D	4			11.12
Reaction	A	n	E	UF
$H + O_2 \leftrightarrow O + OH$	2.64e16	-0.67	71.30	1.5
$O + H_2 \leftrightarrow H + OH$	4.59e4	2.70	26.19	1.3
$OH + H_2 \leftrightarrow H + H_2O$	1.73e8	1.51	14.35	2.0
$OH+OH\leftrightarrow O+H_2O$	3.97e4	2.40	-8.83	1.5
$H + H + M \leftrightarrow H_2 + M$	1.78e18	-1.00	0.00	2.0
$H + H + H_2 \leftrightarrow H_2 + H_2$	9.00e16	-0.60	0.00	2.5
$\rm H + \rm H + \rm H_2O \leftrightarrow \rm H_2 + \rm H_2O$	5.62e19	-1.25	0.00	2.0
$\rm H + \rm OH + \rm M \leftrightarrow \rm H_2\rm O + \rm M$	4.40e22	-2.00	0.00	2.0
$\mathrm{H} + \mathrm{O} + \mathrm{M} \leftrightarrow \mathrm{OH} + \mathrm{M}$	9.43e18	-1.00	0.00	3.0
$O + O + M \leftrightarrow O_2 + M$	1.20e17	-1.00	0.00	2.0
$H + O_2 + M \leftrightarrow HO_2 + M$	6.33e19	-1.40	0.00	1.2
$H_2 + O_2 \leftrightarrow HO_2 + H$	5.92e5	2.43	223.85	2.0
$OH + OH + M \leftrightarrow H_2O_2 + M$	2.01e17	-0.58	-9.59	2.5
$HO_2 + H \leftrightarrow O + H_2O$	3.97e12	0.00	2.81	3.0
$HO_2 + H \leftrightarrow OH + OH$	7.49e13	0.00	2.66	2.0
$HO_2 + O \leftrightarrow OH + O_2$	4.00e13	0.00	0.00	1.2
$HO_2 + OH \leftrightarrow H_2O + O_2$	2.38e13	0.00	-2.09	3.0
	1.00e16	0.00	72.51	3.0
$\mathrm{HO}_2 + \mathrm{HO}_2 \leftrightarrow \mathrm{O}_2 + \mathrm{H}_2\mathrm{O}_2$	1.30e11	0.00	-6.82	1.4
	3.66e14	0.00	50.21	2.5
$H_2O_2 + H \leftrightarrow HO_2 + H_2$	6.05e6	2.00	21.76	3.0
$H_2O_2 + H \leftrightarrow H_2O + OH$	2.41e13	0.00	16.61	2.0
$H_2O_2 + O \leftrightarrow HO_2 + OH$	9.63e6	2.00	16.61	3.0
$H_2O_2 + OH \leftrightarrow HO_2 + H_2O$	2.00e12	0.00	1.79	2.0
	2.67e41	-7.00	157.32	2.0

Davis, Joshi, Wang, Egolfopoulos, Proc. Combust. Inst. 30, 2005

**Uncertainty Propagation** 

 Conditions: Stoichiometric Hydrogen-Air Mixture (29.6% H2; 14.8% O2); Temperature: 1000 K; Pressure: 1 atm;

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Non-intrusive LHS Sampling (25 uncertain variables)

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- Non-intrusive LHS Sampling (25 uncertain variables)



DAKOTA UQ Suite from Sandia National Lab. used for this example

Uncertainty Propagation



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**Uncertainty Propagation** 

 UQ provides an effective quantification of the range (and likelihood) of the ignition delay time

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**Uncertainty Propagation** 

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- ► Given that hydrogen chemistry is the simplest possible chose and we still need ≈ 5000 solutions to get an accurate answer (using LHS), two questions remain

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- Good to know, so what?
- Can we do this faster?

Pose the UQ quest as an Inverse Problem

What uncertainty in the reaction rates can we tolerate to ensure that the probability of ignition delay time exceeding 0.25 ms is less than 10%?

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- Can be cast as an optimization problem under uncertainty: find the maximum UF such that the p(IDT > IDT<sub>cr</sub>) < 0.1</p>

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- ► Problem: too many parameters! Focus only on the branching reaction (*H* + 0<sub>2</sub> ↔ *O* + *OH*)

Quantity	Nominal	Optimal
UF Branching Reaction	1.5	1.29
Mean $\tau_{ign}$ [ms]	0.201304	0.198947
$UF \ \tau_{ign}$	1.7054	1.4023
Probability of Failure	0.191	0.100

**Uncertainty Propagation** 



- Overall uncertainty in the IDT is reduced
- Failure probability below critical requirement

The results shown so far use sampling to compute the statistics of the output of interest

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 The problem is characterized by high-dimensionality of the input (*H*<sub>2</sub> chemistry has 25 uncertain factors)

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The results shown so far use sampling to compute the statistics of the output of interest

- The problem is characterized by high-dimensionality of the input (H<sub>2</sub> chemistry has 25 uncertain factors)
- Polynomial chaos methods cannot be applied because of the exponential cost of building tensorial basis functions (recall cardinality \$\mathcal{P}\$ = \frac{(P+d)!}{P!+d!}\$)

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But the key is that NOT all of the inputs are important!

The results shown so far use sampling to compute the statistics of the output of interest

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- ► Polynomial chaos methods cannot be applied because of the exponential cost of building tensorial basis functions (recall cardinality P = (P + d)! P! + d!)

But the key is that NOT all of the inputs are important! We need to use/develop algorithms that discover the true dependency of the solution

High-Dimensional UQ

Extend the concept of Separation of variables to computational methodologies

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High-Dimensional UQ

Extend the concept of Separation of variables to computational methodologies

- Assume  $y_j$  for j = 1, ..., d are the input uncertainties
- Define

 $u(y_1,...,y_d) \approx \sum_{k=1}^r u_1^{(k)}(y_1) \times u_2^{(k)}(y_2) \times \cdots \times u_d^{(k)}(y_d)$ 

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- ▶ Need to discover the functions *u*<sup>(*k*)</sup> and the rank *r*
- We cast it as an optimization problem: Find the lowest possible r which approximates a set of given function evaluations with u<sup>(k)</sup> being polynomials of fixed maximum order

Mean Ignition Delay Time

Reuse the solutions computed in the autoignition example



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Mean Ignition Delay Time



Even with 500 samples the estimate of the mean ignition delay is acceptable (smaller than MC with 14,000)

STD of Ignition Delay Time



Similar results for the variance



STD of Ignition Delay Time



Similar results for the variance

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 Illustrated Uncertainty Propagation: effect of the input uncertainties on the output

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- Demonstrated the concept of ranking of the uncertainties

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...so far

- Illustrated Uncertainty Propagation: effect of the input uncertainties on the output
- Demonstrated the concept of ranking of the uncertainties
- Showed an example of Backward Uncertainty Propagation: from tolerable outputs to acceptable input uncertainties

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Given one example of efficiency gains with modern UQ algorithms

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- Given one example of efficiency gains with modern UQ algorithms

To finish, I want to give you an example of UQ combined with realistic flow simulations...

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Challenges

 Turbulent flow simulations in realistic geometries with detailed kinetic mechanisms are still beyond the reach of computational engineering



PW6000 simulations enabled by the flamelet modeling approach, but still requiring 1000 CPUs

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**UQ** Challenges

- Uncertainties in kinetic mechanisms might still dominate, especially for the prediction of pollutants
- ► It is impossible to perform more than a handful of simulation (O(5))
- Non-intrusive approach (even our fancy LR method) have no hope of success

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Need to be intrusive and connect the physics/mathematics/UQ

Non-intrusive framework



Perform MANY simulations and sample the outputs



### **Reacting Flow Modeling - Flamelet**

- Basic Premise
  - Since scales of chemical reaction are much smaller than the smallest scales of turbulent, a turbulent flame is simply an ensemble of laminar OflameletsO embedded in a turbulent flow field
  - Solve for flame structure independently from the flow field
- Coordinate Transformation
  - Transform to coordinate system attached to the flame

$$(x,y,z) \rightarrow (Z,Z_{\perp})$$

 Neglect all gradients in tangential directions





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$$(x, y, z) \rightarrow (Z, Z_{\perp})$$

- Neglect all gradients in tangential directions
- Resulting equations are a one-dimensional set of reaction-diffusion equations parameterized by the mixture fraction Z
- Solved in advance and tabulated for a given fuel



Oxidizer

### **Reacting Flow Modeling - Governing Equations**

$$\begin{aligned} \frac{\partial \rho}{\partial t} + \frac{\partial \rho u_j}{\partial x_j} &= \mathbf{0} \\ \frac{\partial \rho u_i}{\partial t} + \frac{\partial \rho u_j u_i}{\partial x_j} &= -\frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left[ 2\mu \left( S_{ij} - \frac{1}{3} \delta_{ij} \frac{\partial u_k}{\partial x_k} \right) \right] \\ \frac{\partial Z}{\partial t} + \frac{\partial \rho Z}{\partial x_j} &= \frac{\partial}{\partial x_j} \left[ \rho D \frac{\partial Z}{\partial x_j} \right] \\ T &= T(\rho, p, Z) \quad \rightarrow \quad \text{tabulated} \end{aligned}$$

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### **Reacting Flow Modeling - Governing Equations**

$$\begin{aligned} \frac{\partial \rho}{\partial t} + \frac{\partial \rho u_j}{\partial x_j} &= 0\\ \frac{\partial \rho u_i}{\partial t} + \frac{\partial \rho u_j u_i}{\partial x_j} &= -\frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left[ 2\mu \left( S_{ij} - \frac{1}{3} \delta_{ij} \frac{\partial u_k}{\partial x_k} \right) \right]\\ \frac{\partial Z}{\partial t} + \frac{\partial \rho Z}{\partial x_j} &= \frac{\partial}{\partial x_j} \left[ \rho D \frac{\partial Z}{\partial x_j} \right]\\ T &= T(\rho, p, Z) \quad \rightarrow \quad \text{tabulated} \end{aligned}$$

- Uncertainty in the kinetic rates appears indirectly through the density
- Use the flamelet equations to ÒconditionÓ the high-dimensional uncertainty
- Can use efficient UQ methods requiring few full system simulations

Intrusive framework



- Split the flamelet-generation part from the actual flow simulations
- Propagate the uncertainty through the flamelet
- Inject uncertainties in the link between flamelets and flow equations (via mixture fraction, density, etc.)

Sandia Flame D

### Piloted partially premixed methane/air flame

- Used NGA (low Mach, structured grid)
- GRI 3.0 mechanism
- Uncertainties in rates from Sheen et al. 2009

#### Simulations

- 1. Used LHS sampling for flamelets (10,000 solutions)
- Compiled tables with mean and variances of density (other uncertainties, e.g. viscosity ignored for now)
- 3. Performed 7 LES simulations sampling on the density distribution



Sandia Flame D

#### Step 1

From kinetic rate uncertainties to flamelet output uncertainties



Rich part of the flame more uncertain

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Sandia Flame D

#### Step 2 Create a stochastic flamelet table



Distributions are Gaussian-like

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#### Step 3 LES with stochastic flamelet table



Emission uncertainty is quite high, and might be comparable with other uncertainties (steady flamelet assumption, kinetic mechanism, etc.)



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